

Congrès Français de Mécanique

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Recueil des Articles



Editorial

Bonjour à tous,

Nous sommes heureux de vous accueillir pour cette 25^e édition du Congrès Français de Mécanique (CFM) en 2022. Un grand nombre de scientifiques français et francophones des universités et des entreprises sont attendus pour cette édition.

Après une tentative d'organiser cette conférence 2021 reportée à cause du COVID, nous pouvons enfin nous retrouver. C'est donc avec un grand plaisir que nous vous accueillons à Nantes qui pour la deuxième fois héberge le Congrès Français de Mécanique. La première édition à Nantes était en 1987. Le CFM est un lieu d'échange, de partages entre les chercheurs. Pour favoriser vos échanges, nous avons décidé d'organiser cette édition du CFM à la cité des Congrès de Nantes. Ainsi dans ce lieu unique, vous pourrez échanger soit entre les sessions ou lors des pauses cafés.

Cette édition du CFM est composée de 35 sessions et d'un mini-symposium. Pour la première fois, le Congrès Français de Mécanique offre une session dédiée à la place des femmes en Mécanique. Cette session s'intéressera aux conséquences sur la vie et la carrière des femmes engagées en Mécanique et sur le manque d'appétence des filles pour les Sciences, les Technologies, l'ingénierie et les Mathématiques. Pendant cette 25^e édition du CFM, un mini-symposium dédié aux doctorants et jeunes docteurs en Mécanique afin d'informer et d'échanger sur la valorisation du doctorat en Mécanique est organisé. Ce mini-symposium est sous l'égide de l'Association du Réseau des Ecoles Doctorales en Sciences pour l'Ingénieur (REDOC-SPI).

Des cours en amont de la conférence ont été proposés. Quatre cours intitulés " Surfaces immatérielles en mécanique et en physique : description théorique et numérique ", " Méthodes hybrides RANS/LES pour la turbulence: théorie et applications ", " Transport Phenomena in Complex Fluids " et " Génération de maillages - Passé-Présent-Futur " ont été proposés le samedi après-midi et le dimanche matin avant le CFM. Ces cours ont rencontré un véritable succès car 45 étudiants ont suivi ces cours.

Enfin, Nantes présente de nombreux centres d'intérêts. Une façon originale de découvrir la ville est de suivre la ligne verte qui vous permettra de découvrir la ville à travers une multitude de propositions culturelles.

Au nom de l'ensemble du comité d'organisation et du comité scientifique, nous vous souhaitons un excellent congrès.

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Table des Matières

Editorial	3
Comité scientifique	3
Comité d'organisation	4
Table des Matières	1
S1 – Procédés de fabrication et de mise en forme par grandes déformations	33
Principes et potentialités du test de formabilité à hautes températures EForT, application à l'étude de la forgeabilité de l'Inconel 625, J. GUERIN, C. DURAND, P. MOREAU, L. FREUND, J. LA BARBERA, E. PUCHI CABRERA, R. BIGOT, L. DUBAR	34
Analyse expérimentale et numérique de la striction d'un matériau " dur " dans un composite colaminé, I. MKINSI, C. BERDIN, A. HELBERT, T. BAUDIN . .	45
Evaluation de la performance environnementale du procédé de thermoformage-estampage de pièces composites en polysulfure de phénylène renforcé par des fibres de carbone (PPS/CF), V. LACOMA	55
Improvement for both ends of the bead in wire-arc additive manufacturing, Z. WANG, S. ZIMMER-CHEVRET, F. LÉONARD, G. ABBA	63
Développement d'un essai de cisaillement séquencé, cisaillement simple - usinage des bords libres, X. COLON, B. GLAPIN, V. GROLLEAU	69
COMPORTEMENT MECANIQUE DU LAITON DE CARTOUCHERIE, B. HAEFFLER, R. DUPUIS	75
Modélisation d'une presse à vis pour la prédiction de l'efficacité lors du forgeage, C. DURAND, C. BAUDOIN, H. SONG, R. BIGOT	90
Vers l'asservissement du pilotage en énergie d'une opération de forgeage : développement d'un métamodèle prédictif pour un jumeau numérique, D. URIBE, C. BAUDOIN, C. DURAND, R. BIGOT	101
S'adapter aux variabilités en cours de processus : développement de métamodèles pour l'obtention de préformes d'estampage, S. FAYS, T. BALAN, L. LANGLOIS, C. BAUDOIN, M. BORSENERGER, R. BIGOT	115
Exploitation of the additive manufacturing process to produce replacement Knee Exoprostheses, N. BEN HARIZ, A. BOULILA, M. AYADI, S. FATTOUCH . . .	122
Nouveaux motifs dans l'impression 3D d'argile, A. GEFFRAULT, H. BESSAIES-BEY, N. ROUSSEL, P. COUSSOT	133

étude d'une condition aux limites simple pour un écoulement à surface libre en rotation dans une cavité cylindrique : effet de la variation du rapport de forme., A. FAUGARET, L. MARTIN WITKOWSKI	1158
Thermomagnetic convective instabilities in the Taylor-Couette ferrofluid flow., A.M. HIREMATH, A. MEYER, H. YOSHIKAWA, I. MUTABAZI	1170
Systematically probing a subcritical dynamo, P. MANNIX	1177
Stabilité temporelle de l'écoulement de Poiseuille plan pulsé à grande amplitude et effet du profil de pulsation, G. ANDRIANO, C. CAILLOL, P. PASSAGGIA, P. HIGELIN	1187
Helmholtz resonator analogue for water waves, L. EUVÉ, P. PETITJEANS, A. MAUREL, V. PAGNEUX, K. PHAM	1201
S10 – Ecoulements diphasiques	1208
Scour downstream of a sluice gate using SedFoam and FLOW-3D, A. GHZAYEL, A. BEAUDOIN	1209
CFD simulation of compressible two-phase flow with high-order methods in NSMB, A.K. GUN, E. GONCALVES, Y. HOARAU	1213
Caractérisation d'écoulements diphasiques eau-air par IRM, D. STEMMELEN, A. OLIVEIRA, S. LECLERC, M. LELONG, A. ARCHER	1221
Approche Front-Tracking pour la modélisation de la rupture et de la coalescence, P. REGNAULT, S. VINCENT, E. CHÉNIER	1232
Écoulement horizontal gaz-liquide intermittent : Faut-il considérer les régimes à poches et bouchons comme deux régimes distincts?, A. ARABI, A. AZZI, A. ZEGHLOUL	1241
Spontaneous oscillations of a growing pendant drop, H. HUANG	1253
Procédé de génération d'une atmosphère polluée contrôlée pour l'étude de la qualité de l'air habitacle des véhicules, H. NADIR	1259
Characterisation of the ventilation in a Taylor-Couette setup with surface piercing riblets, A. CLEMENT, B. BARABE, C. GABILLET	1277
études numérique et expérimentale de l'écoulement engendré par la compression d'air dans un piston liquide, E.M. GOUDA, M. BENAOUICHA, T. NEU, Y. FAN, L. LUO, P. VERGNOL	1289
On the transportation of drill cuttings in prospecting wells under high pressure, high temperature conditions to investigate the performance of the petroleum drilling operation: application to well 10, T.H.Y. NGUYEN, V.T. NGUYEN, S. GUILLOU	1302
Strong interaction between a gas bubble and a free surface in a Hele-Shaw cell at low pressure, N. GRENIER, M. DULUC	1310
Dynamics of the collapse of bubbles in contact with walls, M. SAINI, D. FUSTER, S. ZALESKI	1318
Oscillations of a micro bubble under a free interface, G. DUSSUYER, D. LEG- ENDRE, D. SOTO	1323

2D model to investigate cuttings transport in deviated well: application to the 10-P HTHP well, Cuu Long Basin, Vietnam

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Abstract

Cuttings transport investigation is a mandatory demand in petroleum engineering to estimate performance of hole cleaning due to its significant role in ensuring a prosperous drilling operation, especially in the case of deviated well with complex geometry. Thus, we aim to study the removal of cuttings in a horizontal double-curve well with reference to the prospecting HPHT well 10-P located in Cuu Long basin, Viet Nam. The 2D Euler-Euler model is utilised to model the two-phase flow where the drilling mud is considered non-newtonian and the solid phase is treated as a continuous phase. The numerical models are then validated with theoretical Larsen models. Results of the calculation enable us to predict accumulations of cuttings at different sections of the wellbore.

Résumé

Le transport de déblais de forage est un sujet d'étude incontournable pour l'industrie pétrolière, pour évaluer les performances de nettoyage de trou de forage et garantir la bonne marche des opérations de forage, en particulier dans le cas de puits de forage courbes et de géométries complexes. Ainsi nous abordons l'étude de l'enlèvement de déblais de forage dans un puits horizontal à double courbe, avec comme référence le puits de prospection HPHT 10-P situé dans le bassin de Cuu Long au Viet Nam. Le modèle 2D Euler-Euler est utilisé pour modéliser l'écoulement diphasique où la boue de forage est considérée comme un fluide non-newtonien et la phase solide considérée comme continue. Les modèles numériques sont alors validés par comparaison aux modèles théoriques de Larsen. Les résultats permettent de prédire l'accumulation de déblais de forage à différentes sections.

Key words: Cuttings transport, HTHP, deviated well, Euler-Euler

1. Introduction

In petroleum drilling, drilling mud play its role as a conduct to transport rock fragments, induced during the penetration of the drill-bit into the earth's crust, upwards to the surface, fig 1.1. A poor hole cleaning performance may cause aggressive accumulation of cuttings at low side of the wellbore, which is considered a root cause of several problems to the drilling operation such as stuck pipe [1],[2],[3]

especially in deviated well. The efficiency of the cuttings transport depends greatly on operational parameters such as: mud pump flowrate which decides the annular velocity of the upward flows [14], [15]; rheology the drilling fluid which plays a very important part in removing cuttings, especially in highly inclined and horizontal wells [16], [14]; hole inclination which affects the process to evacuate cuttings out of the drilling well [13] and ROP (rate of penetration) and pipe rotation (rpm) which take their effects on the cleaning efficiency by reducing cuttings deposition and preventing the accumulation of the cuttings bed [13], [11], and properties of cuttings. Various numerical and experimental studies have been carried out to estimate effects of influential parameters on the performance of cuttings transport with applications to horizontal, vertical or inlined wells independently. However, very few considered a deviated well trajectory completely. Therefore, we aim in our research to create a two-phase 2D model to investigate the removal of cuttings in a 5-section deviated well. The calculating domain is constructed as a reduced model referring to the well 10-P in Culong Basin, Vietnam. This well is known as a horizontal double-curve well, in which its trajectory composes of 3 major sections including: a) vertical section from spuding, b) inclined part after the first kick-off point and c) approximately horizontal section to reach to the objective reservoir, *figure 1.2*. We expect to obtain a panoramic view of the whole circulating process through this complex domain, that is absent from mostly all research on drill cuttings transport.

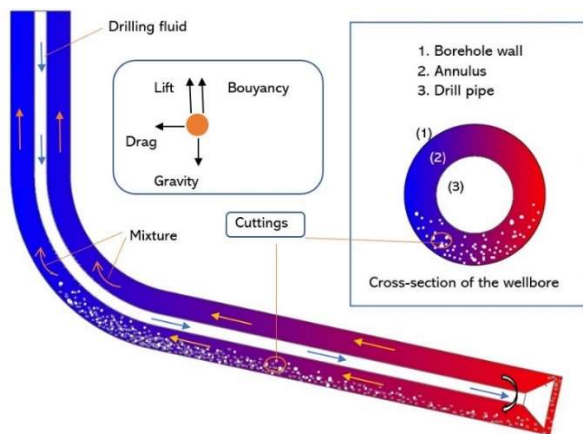


Figure 1.1. Two-fluid flow inside a drilling well

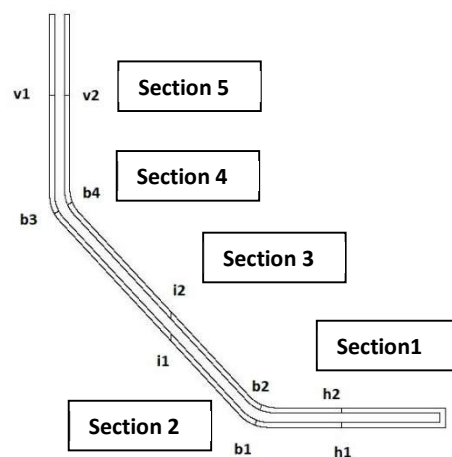


Figure 1.2. Reduced cuttings transport model with reference to the horizontal double-curve well, 10-P

2. Methodology

Gas phase and bubble are neglected in this work, thus, the flow coming upward consists of two phases: drilling mud (fluid phase) and cuttings (solid phase). Where, the drilling fluid is considered as a homogenous water-based mud with no additives added to gain desired rheology. The Euler-Euler (EE) model is adopted to solve this multiphase flow in the interest of saving time [9] while providing trustable results.

According to ANSYS Fluent, mathematical formulations for EE model are written in form of Continuity equation, Fluid-fluid momentum equation and fluid-solid momentum equation:

* Continuity:

$$\frac{1}{\rho_c} \left(\frac{\partial}{\partial t} (\alpha_c \rho_c) + \right) + \nabla \cdot (\alpha_c \rho_c \vec{v}_c) = \sum_{m=1}^N (m_{mc} - m_{cm}) \quad (2.1)$$

* Fluid-fluid momentum equation:

$$\frac{\partial}{\partial t}(\alpha_m \rho_m \vec{v}_m) + \nabla \cdot (\alpha_m \rho_m \vec{v}_m \vec{v}_m) = -\alpha_m \nabla p + \nabla \cdot \bar{\tau}_q + \alpha_m \rho_m \vec{g} + \sum_{c=1}^N (K_{mc}(\vec{v}_m - \vec{v}_c) + \dot{m}_{mc} \vec{v}_{mc} - \dot{m}_{cm} \vec{v}_{mc}) + (\vec{F}_m + \vec{F}_{lift,m} + \vec{F}_{vm,m} + \vec{F}_{td,m}) \quad (2.2)$$

* Fluid – solid momentum equation:

$$\frac{\partial}{\partial t}(\alpha_c \rho_c \vec{v}_c) + \nabla \cdot (\alpha_c \rho_c \vec{v}_c \vec{v}_c) = -\alpha_c \nabla p - \nabla p_s + \nabla \cdot \bar{\tau}_q + \alpha_c \rho_c \vec{g} + \sum_{m=1}^N (K_{mc}(\vec{v}_m - \vec{v}_c) + \dot{m}_{mc} \vec{v}_{mc} - \dot{m}_{cm} \vec{v}_{mc}) + (\vec{F}_c + \vec{F}_{lift,c} + \vec{F}_{vm,c} + \vec{F}_{td,c}) \quad (2.3)$$

Where, \vec{v}_m and \vec{v}_c are velocity of the drilling mud (fluid phase) and cuttings (solid phase) respectively; ρ_m and ρ_c are densities of the two phases.

The flows are expected to be turbulent, thus, the k-e viscous model is activated. The well 10-P is drilled in high pressure, high temperature (HPHT), ie., $T \sim 150 \div 205^\circ\text{C}$ and $P \sim 10.000 \div 20.000$ psi). To consider these features, the mud flow is treated as non-Newtonian fluid. Fluent enables us to approximately characterize the fluid phase as non-Newtonian fluid by using power-law (PL) rheology model, Herschel-Bulkley or Carreau model [12,13]. For the sake of simplicity, PL model is utilised.

Using EE approach, particle phase is regarded as continuous phase and set as granular flow which obeys the granular viscosity model suggested by Syamlal et al, 1993. An estimation of the particles injection velocity has been made basing on the penetration rate (ROP). The experimental Larsen model [5],[6],[7],[8],[10], which describes relation between cutting velocity V_c and the rate of penetration ROP as in the equation (Eq.(2.4)), is employed to validate numerical results.

$$V_c = \frac{ROP}{36 \left[1 - \left(\frac{D_p}{D_h} \right)^2 \right] C_c} \quad (2.4)$$

Where, D_p represents diameter of cuttings, D_h is the diameter of the borehole, C_c is the concentration factor of cuttings.

Calculation data is recapitulated in the following table, *table 1*.

Table 1. Calculation data

Parameters	Testing values
Diameter of drillpipe, D_p , m	0.2
Diameter of wellbore, D_h , m	0.4
Distance between wellbore and drillpipe, r_i , m	[0:0.15]
Mud density, ρ (γ), kg/m^3	1010; 1050; 1200;1300
Velocity of mud, V_f , m/s	0.04;0.08; 0.2; 0.4; 0.8; 1.0
Cuttings density, kg/m^3	2600
Cuttings dimension, D_c , m	0.001; 0.005;0.01
Cuttings velocity, V_c , m/s	0.008
Temperature, $^\circ\text{C}$	150
Pressure, psi	12000
Turbulent intensity	8%

As can be seen in the table, quantities of cuttings size, velocity of the drilling fluid and mud density vary respectively each by each in different test cases. The set of values, $V_f = 0.4$ m/s; $D_c = 0.001$ m; $V_c = 0.08$ m/s, $\gamma = 1010$ kg/m^3 is taken as reference data (the same values as data measured at the actual well 10-P).

3. Results

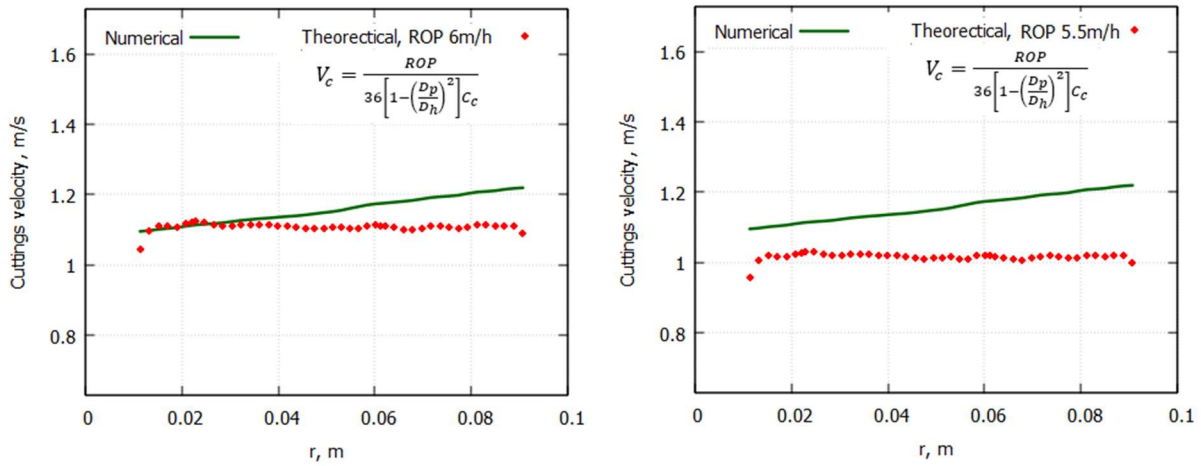


Figure 3.1. Theoretical vs numerical cuttings velocity, ROP = 5.5 and 6.0m/s (section 2)

Preliminary calculations were first carried out using reference data. The numerical cuttings velocity is presented in figure 1 in comparison with cuttings velocity, V_c , calculated from eq. (2.4). As observed, numerical model shows a tendency to increase the magnitude of cuttings velocity, especially in the case of lower ROP. However, the result is considered acceptable due to the difference in geometry between our calculating domain and the actual well. Thus, the model is used for further calculations. In the current research, two cases of simulation were carried out to investigate dependency of cuttings transport on cuttings size and velocity of the drilling fluid.

Results of calculations are extracted for the two branches of the domain from the bottom to the top as denoted in *figure 1.2*. We consider all 5 sections throughout the calculating domain, two lines at each. *Section 1* with $h1$ and $h2$, is the horizontal part; *section 2* consists of bend 1 (b1) and bend 2 (b2); *section 3* is the inclined part with $i1$ and $i2$ at each branch; *section 4* composes of the two other bends b3 and b4; and *section 5* with $v1$ and $v2$ is vertical section. Length of each line equals $r_i \max = 0.1m$ corresponding to the distance between the borehole wall and the drillpipe as the well is concentric.

* *Study case 1: Dependence of cuttings velocity on cuttings size*

Figure 3.2, 3.3 demonstrates the relation between cuttings size on the transportation of cuttings with the red curve represents velocity of cuttings at the suspension layer and the other in black depicts velocity at the dispersed layer. As observed, cuttings velocity decreases sharply with the increase of cuttings mass and size at all the 5 sections. The higher the size of particle, the smaller the velocity of cuttings, especially at dispersed layer and as a consequence the faster the settling of cuttings and the thicker the cuttings bed. V_c drops to very small values when $D_c = 0.01m$ that enables us to predict a blockage if V_f remains unchanged. However, compare to results published by Shu, 2021, our model seems to overestimate magnitude of velocity in the annulus [16]. In figure 3.3, the concentration of cuttings of different size at 5 different sections is illustrated. As observed, the highest accumulation of cuttings corresponds to the case $D_c = 0.005mm$, not to the case of cuttings with largest diameter $D_c = 0.01m$. This seems to be a paradox at first, however, it's quite logic due to a confirmation that larger cuttings size benefits a higher removal than those of smaller size [17].

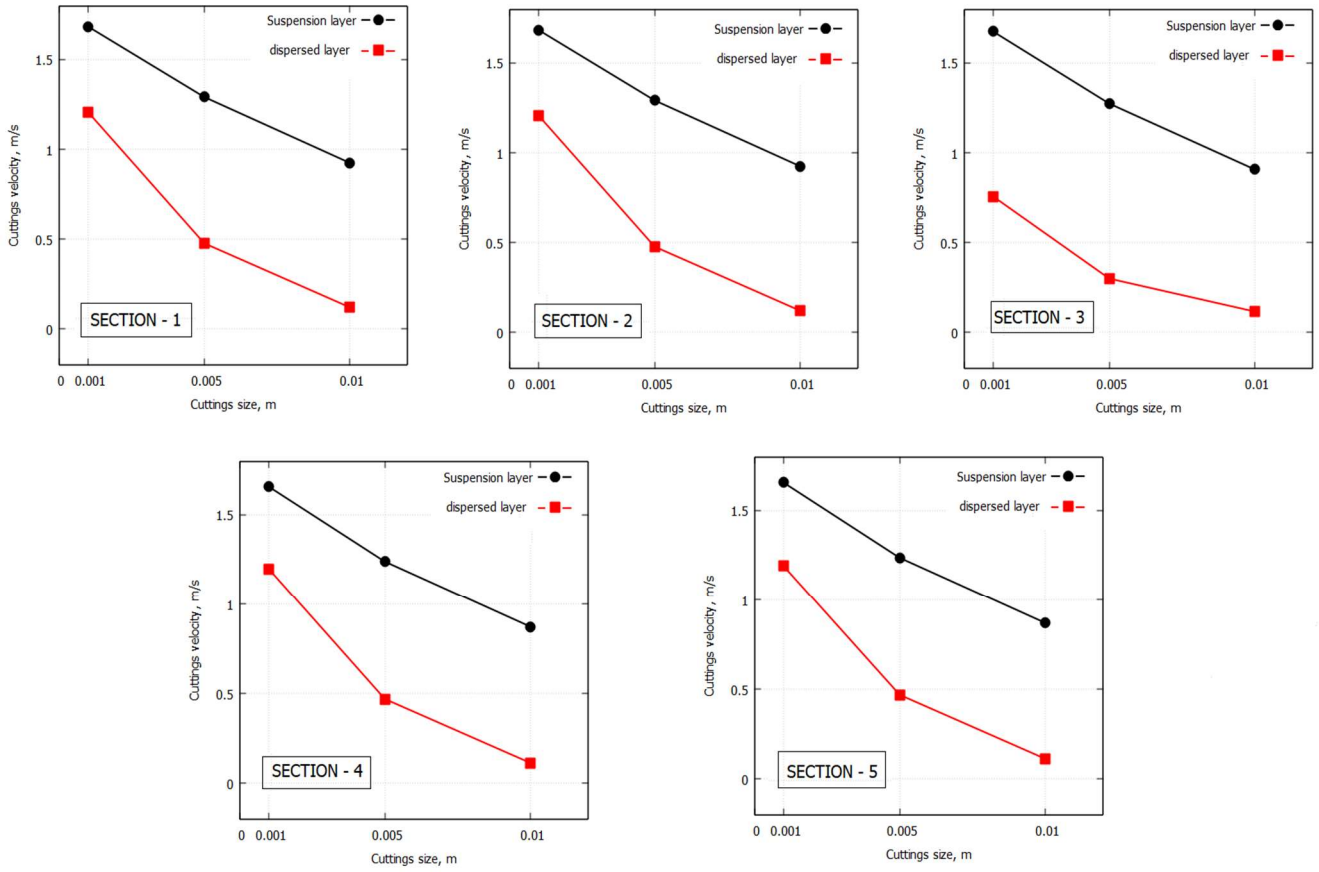


Figure 3.2. Effect of cuttings size D_c on cuttings velocity V_c at 5 sections (V_f at the inlet takes the reference value, $V_f = 0.4$)

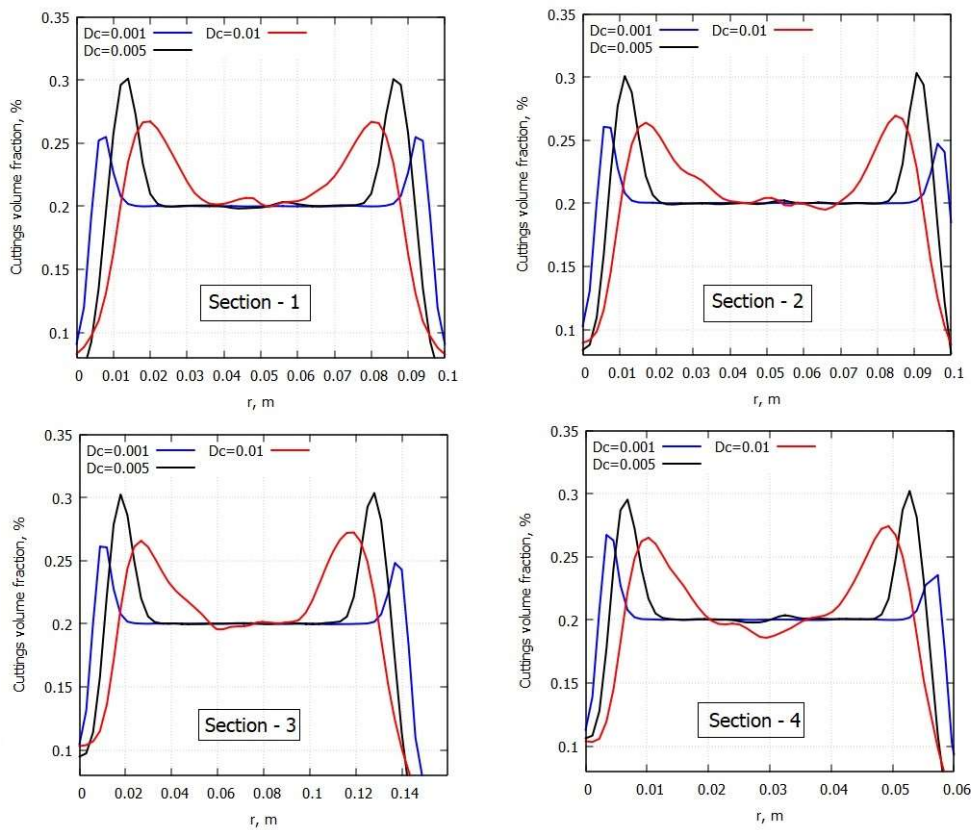


Fig 3.3. Volume fraction of cuttings for different sizes of cuttings, D_c

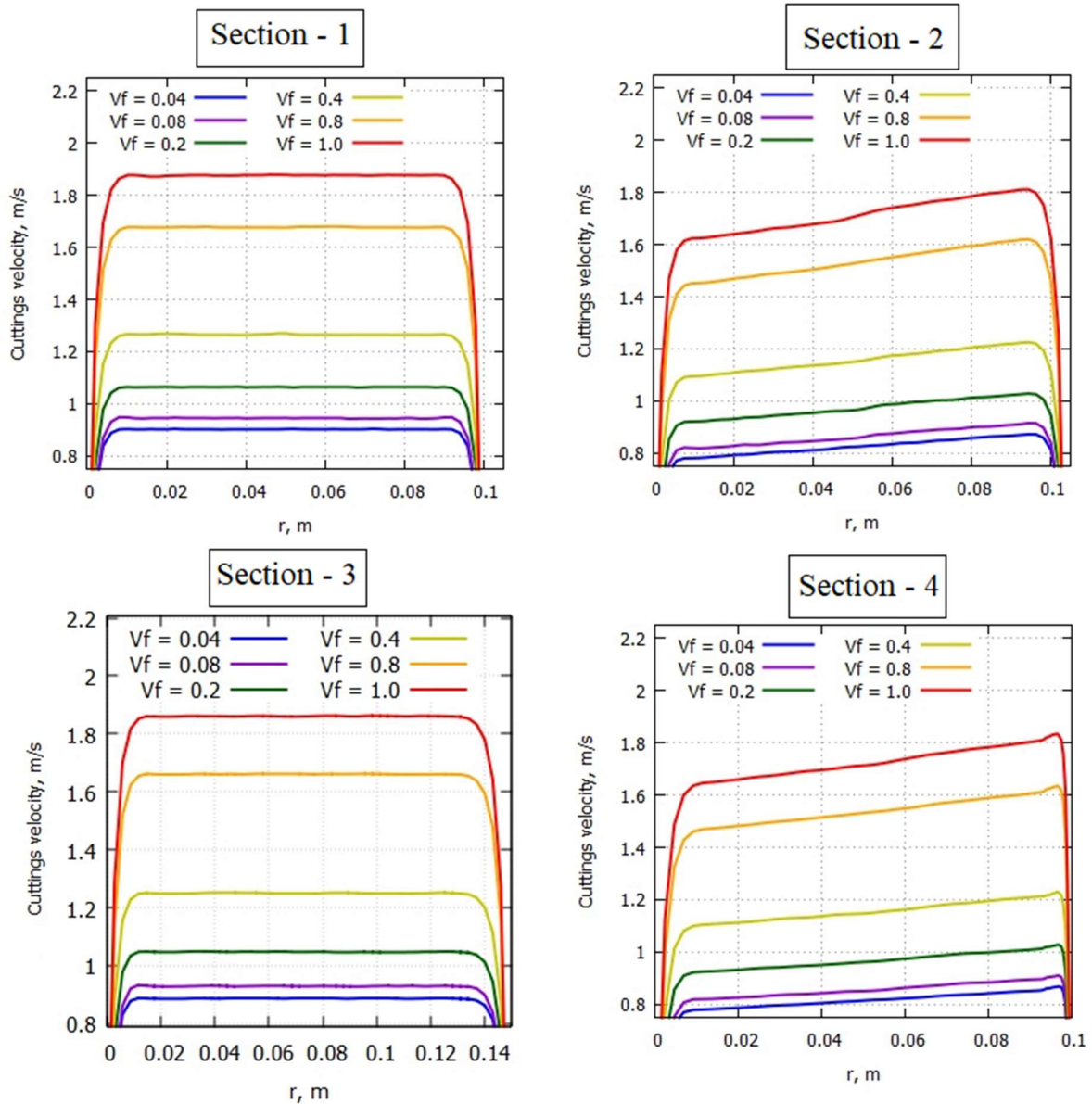


Figure 3.4. Cuttings velocity at different mud speeds

* Study Case 2: Impact of mud velocity on the transportation of cuttings at different sections of the wellbore

Figure 3.4 illustrates cuttings velocity at 5 different sections. Velocity curves seem to be flat and smooth around the center of the pipe, whereas slight fluctuations are observed at the contact areas between the flow and the borehole wall and the pipe. At the two bends (section-2 and section-4), V_c tends to be smaller and linearly increases following the direction from the wellbore to its center. This enables us to confirm a higher risk of cuttings accumulations at the lower sides of the two bends. Besides, it's a doddle to see that higher drilling mud velocity results in higher cuttings velocity. However, a too fast upcoming flow may not be a wise choice due to its capability to cause unstable conditions to the wellbore and formation. Therefore, further calculations should be implemented in order to determine the optimum flowrate to pump down the drilling must obtain maximum hole cleaning performance.

4. Discussion and Conclusion

In this work, 2-dimensional approach using E-E model was carried out to investigate a two-phase liquid-solid (drilling fluid as non-newtonian fluid and cuttings) flow in the annulus. Results show an increase of cuttings concentration at bends in comparison to the other positions of the well. Besides, it confirms a more effective removal with larger cuttings size. Despite of some valuable insight, the researched domain is sketched with two separated parts which leads to no connection between the upper and lower part of the domain except at the bottom. While in fact, drilling fluid and cuttings move upward in the annulus, a void formed when a pipe is positioned inside a bigger one. Consequently, 2D model may overevaluate velocities of the flows at each branch of the domain. Besides, rotary movement (RPM) of the drillpipe was neglected due to asymmetric geometry of the domain which is the biggest minus of the work. Therefore, 3D models are suggested for later calculations to capture 3 dimensional effects and to consider drilling parameters eliminated in the current research.

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